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U.S. Nitric Acid Production Project Data Report

The Project Data Report (PDR) Template must be completed for each verification period. This template is only intended as a guide and provides the minimum required information to be reported. This template is designed for use with the Nitric Acid Production Protocol V2.2 and V3.0. The project developer has the option to include additional information at their discretion.

Please note that this document will be made publicly available once the project has registered credits for the verification period. If there is proprietary information, please provide a redacted version for publication and a non-redacted version for internal review. Please contact the Reserve to discuss what information may be allowed to be redacted.

Account Holder	Dyno Nobel Inc.
Project ID and Name	CAR2060 Dyno Nobel LoMo NAP
Cooperative/Aggregate ID (if applicable)	N/A
Current Reporting Period Dates	11/04/2025 - 07/06/2026
Protocol Version	Nitric Acid Production V3.0
Claimed CRTs by Vintage	2025: 105,428 2026: 361,092
Date Submitted	9/14/2026

1 Introduction

Provide a general description of the project, including location, baseline scenario, project activity, etc.

Dyno Nobel Inc. (Dyno Nobel) manufactures commercial explosives. The purpose of this project is to reduce nitrous oxide (N₂O) emissions from the Dyno Nobel LoMo NAP in Louisiana, Missouri. The project involves the installation of a new catalyst in the tail gas leaving the absorption tower (a “tertiary catalyst”) for which the sole purpose is the decomposition of N₂O. Abatement system is a tertiary abatement catalyst at the Louisiana, Missouri facility. The technology deploys a tertiary catalyst system downstream of the ammonia oxidation reactor, decomposing the nitrous oxide that would have otherwise been vented to the atmosphere.

2 Project Definition

a Project Definition

Describe the abatement technology used, and confirm that the following scenarios do not apply to the project:

- *NAPs that are restarted any time after December 2, 2007, after being out of operation for a period of 24 months or longer*
- *New NAPs constructed after December 2, 2009, with the exception of new NAPs for which a permit application for construction was submitted to the appropriate government authorities prior to December 2, 2009*
- *Secondary catalyst projects at existing NAPs where NSCR is currently operating*
- *Secondary catalyst projects at existing NAPs that used NSCR technology for NO_x abatement at any point since December 2, 2007*

A tertiary catalyst system is used downstream of the ammonia oxidation reactor. The above scenarios do not apply to the project.

b Project Developer

List the entities which have any amount of legal control over the project boundary and identify the mechanism through which the Account Holder has legal authority to implement the project. In addition, please state which entity will be designated as the project developer and will sign the Attestation of Title. If the Account Holder is not the entity listed on the facility’s operating permit, explain how they obtain the right to operate the project on the facility’s behalf. which entity will be designated as the project developer and will sign the Attestation of Title. If there are no technical consultants or other parties with material interest, state “N/A.”

Current Project Participants include the Offset Project Operator, ClimeCo LLC (ClimeCo) and the Project Facility Owner/Operator, Dyno Nobel Inc. (Dyno Nobel). Dyno Nobel is the exclusive owner of the project and the sole party with the right to make management and operational decisions. Dyno Nobel serves as the owner and operator of the tertiary abatement catalyst system, personal property, equipment, fixtures and appurtenances comprising the Project.

Technical Consultant(s): ClimeCo LLC.

Other Parties with Material Interest (entity name and role): N/A

Entity Signing Attestation of Title: Dyno Nobel Inc.

Additional Information:

3 Project Eligibility

a Project Location

Provide the project location.

The project is located in Louisiana, Missouri, USA.

b Project Start Date

For secondary projects, the project start date is the date on which production first commences after the installation of a secondary catalyst. Confirm the start date is either the start of a campaign or the commencement of nitric acid production after an outage. For tertiary projects, the project start date is the date on which production first commences after installation of a tertiary catalyst. Projects that switch abatement technologies or installs an additional system for a combined secondary and tertiary catalyst project the start date should correspond with the original start date from the initial listing.

Please provide the start date for the project and describe the documentation used to demonstrate the start date as described above. Provide the duration of the project startup testing, if applicable.

The project was submitted on 03/14/2025, project start date was 12/09/2024.

c Project Crediting Period

Due to the nature of campaigns, a crediting period for nitric acid production projects is approximately ten years and aligns with the end of the last full campaign that begins in the tenth year of reporting. If the project developer anticipates a crediting period greater than 11 years in total, provide the date in which the project received Reserve approval prior to the initiation of the final campaign.

Provide the crediting period below using an approximate date for the crediting period end date.

12/09/2024 to approximately 12/08/2034

Date of Reserve Approval if applicable:

d Additionality

i Performance Standard Test

The Performance Standard Test for Nitric Acid Production projects is based on an assessment of common practice of use of emission control technologies in NAPs to reduce N₂O emissions. Check the box below for how the project meets the Performance Standard Test.

☐ Secondary catalyst

☒ Tertiary catalyst, including catalytic decomposition or NSCR

☐ Combined secondary and tertiary catalyst

ii Legal Requirement Test

Attest that the project activities are not legally required. Identify any federal, provincial, or local regulations or legally binding mandates that are relevant to the project.

There are currently no regulatory requirements for the abatement of N₂O resultant from the nitric acid production process. The technology installed within the scope of the project meets and exceeds industry standard practices. We have confirmed that there are currently no laws requiring the abatement of N₂O at the plant. In addition, Dyno Nobel monitors any change in regulations that may affect eligibility.

e Social and Environmental Safeguards**i Social Safeguards**

Confirm below that the project is in material compliance with all labor and safety laws for the verification period.

There have been no instances of non-compliance with labor or safety laws within the nitric acid plant that relate to the project for the verification period.

ii Environmental Safeguards

Confirm below that the project is in material compliance with all environmental regulations in the verification period, and how the project is designed and implemented in such a way to mitigate potential releases of pollutants that may cause degradation of the quality of soil, air, and surface and groundwater.

The project is in material compliance with all environmental regulations in the verification period. The project owner retains a technical consultant (ClimeCo) to monitor state and federal legislation, as well as the publicly available information on non-compliance events posted on the US EPA databases.

f Regulatory Compliance

Provide the federal, state, and/or local regulatory agencies with jurisdiction over the project boundary. Disclose any instances of non-compliance during the verification period. Describe how the project intends to monitor for compliance during future reporting periods.

The US EPA and OSHA have jurisdiction over the project boundary. A survey of all regulatory violations incurred by the Site within the reporting period dates has been conducted as part of verification activity and submitted for the verifier's review. There are no regulatory violations for this reporting period that have been caused by project activity.

A review of EPA ECHO stated a CWA violation from Q1 2026. This was related to an audit conducted in 2026 related to the last two years of Discharge Monitoring Reports, where a permit exceedance occurred in 2024, which was appropriately reported and resolved. Minor typos in the reports were also corrected, which is the incorrect reporting quarter listed on ECHO. The NPDES permit is outside the project boundary and is related to dates outside the project reporting period.

The Missouri DNR Environmental Incident database reported an incident on 6/18/2026, however this was related to a neighboring plant a mile down the road and is not related to the facility or the project activity in any way.

4 GHG Assessment Boundary

a GHG Assessment Boundary

The table below includes only the SSRs that are included in the project quantification. For all SSRs considered in the GHG Assessment Boundary (included and excluded GHGs and their justification) refer to Tables 4.1 and 4.2 in the Protocol.

Secondary Catalyst Projects

SSR	Source Description	Gas	Baseline (B) or Project (P)
1 – Nitric Acid Production	Nitric acid process unit (burner inlet to stack)	N ₂ O from reaction byproduct	B, P

Tertiary Catalyst Projects

SSR	Source Description	Gas	Baseline (B) or Project (P)
1 – Nitric Acid Production	Nitric acid process unit (burner inlet to stack)	N ₂ O from reaction byproduct	B, P
4 - Ammonia Used to Operate SCR De-NOX Unit (included if ammonia is an input to the N ₂ O destruction facility)	GHG emissions from production of ammonia used in tertiary abatement for N ₂ O destruction	CO ₂ , CH ₄ , N ₂ O	B (if applicable), P
5 - Hydrocarbon Input	Hydrocarbon used as reducing agent and/or reheating the tail gas	CO ₂ and/or CH ₄	P
7 - External Energy to Reheat Tail Gas	May be used to reheat the tail gas before entering the tertiary catalyst or NSCR	CO ₂ , CH ₄ , N ₂ O	P

Combined Secondary and Tertiary Catalyst Projects

SSR	Source Description	Gas	Baseline (B) or Project (P)
1 – Nitric Acid Production	Nitric acid process unit (burner inlet to stack)	N ₂ O from reaction byproduct	B, P

4 - Ammonia Used to Operate SCR De-NOX Unit (included if ammonia is an input to the N ₂ O destruction facility)	GHG emissions from production of ammonia used in tertiary abatement for N ₂ O destruction	CO ₂ , CH ₄ , N ₂ O	B (if applicable), P
5 - Hydrocarbon Input	Hydrocarbon used as reducing agent and/or reheating the tail gas	CO ₂ and/or CH ₄	P
7 - External Energy to Reheat Tail Gas	May be used to reheat the tail gas before entering the tertiary catalyst or NSCR	CO ₂ , CH ₄ , N ₂ O	P

5 Quantifying GHG Emission Reductions

a Quantifying Baseline Emissions

i Summary of Baseline Quantification

Provide the following information depending on the project scenario. Provide the following information depending on the project scenario. Leave the other section blank if not applicable.

Secondary Catalyst Projects

Allowable Operating Conditions:

Oxidation temperature range:

Oxidation pressure range:

Maximum ammonia-to-air ratio input into the AOR:

Select how these allowable ranges were determined:

- ☐ Option (a): The best available historical data for the operating range of temperature and pressure, and maximum ammonia-to-air ratio from the previous five campaigns.
- ☐ Option (b): The best available historical data from less than five campaigns. This option is allowable only if limited historical data are available (e.g., an upgraded or relocated NAP that has not been operating for at least five campaigns).
- ☐ Option (c) Specified range of temperature and pressure found in the operating manual²⁰ for the existing equipment, and maximum ammonia-to-air ratio as specified by the ammonia oxidation catalyst manufacturer or the operating manual for the NAP equipment if guidance from the ammonia oxidation catalyst manufacturer is not available. This option is only allowable if no historical data are available.

Vintage:	Vintage:
HNO ₃ ,MAX, scaled: tHNO ₃	HNO ₃ ,MAX, scaled: tHNO ₃
Baseline Emission Factor: tN ₂ O/tHNO ₃	Baseline Emission Factor: tN ₂ O/tHNO ₃
Total N ₂ O Emissions during the Baseline Sampling Period: tN ₂ O	Total N ₂ O Emissions during the Baseline Sampling Period: tN ₂ O
Baseline Emissions: tCO ₂ e	Baseline Emissions: tCO ₂ e

Tertiary Catalyst Projects

Allowable Operating Conditions:

Oxidation temperature range: 825°C - 925°C

Oxidation pressure range: 125 PSIG - 175 PSIG

Maximum ammonia-to-air ratio input into the AOR: 21%

Select how these allowable ranges were determined:

- ☒ Option (a): The best available historical data for the operating range of temperature and pressure, and maximum ammonia-to-air ratio from the previous five campaigns.
- ☐ Option (b): The best available historical data from less than five campaigns. This option is allowable only if limited historical data are available (e.g., an upgraded or relocated NAP that has not been operating for at least five campaigns).
- ☒ Option (c) Specified range of temperature and pressure found in the operating manual²⁰ for the existing equipment, and maximum ammonia-to-air ratio as specified by the ammonia oxidation catalyst manufacturer or the operating manual for the NAP equipment if guidance from the ammonia oxidation catalyst manufacturer is not available. This option is only allowable if no historical data are available.

Vintage: 2025	Vintage: 2026
HNO ₃ ,MAX, scaled: 89,318 tHNO ₃	HNO ₃ ,MAX, scaled: 305,916 tHNO ₃
Baseline Emission Factor: N/A tN ₂ O/tHNO ₃	Baseline Emission Factor: N/A tN ₂ O/tHNO ₃
Total N ₂ O Emissions during the Baseline Sampling Period: N/A tN ₂ O	Total N ₂ O Emissions during the Baseline Sampling Period: N/A tN ₂ O
Baseline Emissions: 107,078 tCO ₂ e	Baseline Emissions: 366,744 tCO ₂ e

Combined Secondary and Tertiary Catalyst Projects

Allowable Operating Conditions:

Oxidation temperature range:

Oxidation pressure range:

Maximum ammonia-to-air ratio input into the AOR:

Select how these allowable ranges were determined:

- ☐ Option (a): The best available historical data for the operating range of temperature and pressure, and maximum ammonia-to-air ratio from the previous five campaigns.
- ☐ Option (b): The best available historical data from less than five campaigns. This option is allowable only if limited historical data are available (e.g., an upgraded or relocated NAP that has not been operating for at least five campaigns).
- ☐ Option (c) Specified range of temperature and pressure found in the operating manual²⁰ for the existing equipment, and maximum ammonia-to-air ratio as specified by the ammonia oxidation catalyst manufacturer or the operating manual for the NAP equipment if guidance from the ammonia oxidation catalyst manufacturer is not available. This option is only allowable if no historical data are available.

Vintage:	Vintage:
HNO _{3,RP, scaled} : tHNO ₃	HNO _{3,RP, scaled} : tHNO ₃
EF _{BL} : tN ₂ O/tHNO ₃	EF _{BL} : tN ₂ O/tHNO ₃
HNO _{3,NEW} : tHNO ₃	HNO _{3,NEW} : tHNO ₃
EF _{NEW} : tN ₂ O/tHNO ₃	EF _{NEW} : tN ₂ O/tHNO ₃
Baseline Emissions: tCO _{2e}	Baseline Emissions: tCO _{2e}

b Quantifying Project Emissions

i Summary of Project Emissions

Complete the table below depending on the project scenario. Leave the other table blank if not applicable.

Secondary Catalyst Projects:

Vintage:	Vintage:
Total N ₂ O emissions in the campaign: tN ₂ O	Total N ₂ O emissions in the campaign: tN ₂ O
Project Emissions: tCO _{2e}	Project Emissions: tCO _{2e}

Tertiary Catalyst Projects:

Vintage: 2025	Vintage: 2026
Emissions from the N ₂ O in the tail gas during the reporting period: 1,650 tCO ₂	Emissions from the N ₂ O in the tail gas during the reporting period: 5,651 tCO ₂
Emissions from the ammonia input used to operate the tertiary catalyst facility during the reporting period: 0 tCO ₂	Emissions from the ammonia input used to operate the tertiary catalyst facility during the reporting period: 0 tCO ₂
Emissions from the use of hydrocarbons as a reducing agent or to reheat tail gas during the reporting period: 0 tCO ₂	Emissions from the use of hydrocarbons as a reducing agent or to reheat tail gas during the reporting period: 0 tCO ₂

Emissions from the external energy used to reheat the tail gas during the reporting period: 0 tCO ₂	Emissions from the external energy used to reheat the tail gas during the reporting period: 0 tCO ₂
Project Emissions: 1,650 tCO ₂ e	Project Emissions: 5,651 tCO ₂ e

Combined Secondary and Tertiary Catalyst Projects – Approach 1:

Vintage:	Vintage:
Emissions from the N ₂ O in the tail gas during the reporting period: tCO ₂	Emissions from the N ₂ O in the tail gas during the reporting period: tCO ₂
Emissions from the ammonia input used to operate the tertiary catalyst facility during the reporting period: tCO ₂	Emissions from the ammonia input used to operate the tertiary catalyst facility during the reporting period: tCO ₂
Emissions from the use of hydrocarbons as a reducing agent or to reheat tail gas during the reporting period: tCO ₂	Emissions from the use of hydrocarbons as a reducing agent or to reheat tail gas during the reporting period: tCO ₂
Emissions from the external energy used to reheat the tail gas during the reporting period: tCO ₂	Emissions from the external energy used to reheat the tail gas during the reporting period: tCO ₂
Project Emissions: tCO ₂ e	Project Emissions: tCO ₂ e

c Final CRT Summary

Summarize the final result for determining the net GHG Reductions by vintage.

Vintage: 2025	Vintage: 2026
Baseline Emissions: 107,078 tCO ₂ e	Baseline Emissions: 366,744 tCO ₂ e
Project Emissions: 1,650 tCO ₂ e	Project Emissions: 5,651 tCO ₂ e
Total GHG Emission Reductions: 105,428 tCO ₂ e	Total GHG Emission Reductions: 361,092 tCO ₂ e

6 Variance Request

If a variance was requested during the verification period, provide a brief description of the rule/requirement in the protocol in question, the conditions of the determination, and the date of the variance request and determination.

Date of Variance Request:

Protocol Section and Rule/Requirement:

Description of how the project did not meet the above requirements:

Date Reserve Issued Determination:

Variance Conditions:

7 Project Documentation

The following documents are required to be submitted for project registration. In cases where there is proprietary information, please provide unredacted and redacted versions. If additional documents were submitted, please include the document title and its associated file name.

Document	File Name
Project Diagram	Dyno Nobel PFD.pptx
Attestation of Title	Attestation-Title-Dyno-RP3.pdf
Attestation of Voluntary Implementation	Attestation-Voluntary-Implementation_ Dyno –RP3.pdf
Attestation of Regulatory Compliance	Attestation-Regulatory-Compliance_ Dyno –RP3.pdf
Monitoring Plan	Dyno Nobel CAR2060 Monitoring Plan v1_1.docx
Project Contributions to the U.N. Sustainable Development Goals Report Tool	2025-2026-SDG-REPORTING-TOOL CAR2060.pdf
Project Data Report (this document)	RP3 CAR2060 Project Data Report_v2.0.pdf
Variance Request (if applicable)	N/A